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Experimental Analysis to Determine Effect of Aspect Ratio on Heat Transfer from Square Taper Fin Array in Natural Convection

Gonavath Devendra Naik

MTech Student Kakinada Institute Of Technology & Science, Divili, Andhra Pradesh, India.

Mr. K.Mohan Krishna

Assistant Professor Kakinada Institute Of Technology & Science, Divili, Andhra Pradesh, India.

Mr. Sanmala Rajasekhar

Associate Professor Kakinada Institute Of Technology & Science, Divili, Andhra Pradesh, India.

ABSTRACT:

Heat transfer from the heat sink plays major role on the performance on various components in different industries like Automobile industries, Air conditioning industries, Heat treatment, Electronic Industries. In this heat transfer process material type, shape, length plays a major role.

In this thesis Thermal and CFD analysis will be conducted on the square fin arrays by natural convection heat transfer process. In this thesis, materials considered are aluminium alloy he 15 and 30. Parameters varied in this work are space between fins, length, and thickness. Experimental work will be conducted in the still air. 3D modeling software CATIA V5 will be used for 3D models of square fin arrays. Thermal and CFD analysis will be done in ANSYS.

Keywords: - Heat transfer, square array

I. INTRODUCTION

The removal of excessive heat from system components is essential to avoid the damaging effects of burning or overheating. Therefore, the enhancement of heat transfer is an import subject of thermal engineering. The heat transfer from surfaces may in general be enhanced by increasing the heat transfer coefficient between a surface and its surroundings, by increasing the heat transfer area of the surface, or by both. In most cases, the area of heat transfer increased by utilizing extended surfaces in the form of fins attached to walls and surfaces Extended surfaces (fins) frequently used in heat exchanging devices for the purpose of increasing the heat transfer between a primary surface and the surrounding fluid.

Fins are surfaces that extend from an object to increase the rate of heat transfer to or from the environment by increasing convection. The amount of conduction, convection, or radiation of an object determines the amount of heat it transfers. Increasing the temperature gradient between the object and the environment, increasing the convection heat transfer coefficient, or increasing the surface area of the object increases the heat transfer. Sometimes it is not feasible or economical to change the first two options. Thus, adding a fin to an object increases the surface area and can sometimes be an economical solution to heat transfer problems.

THE FUNCTION OF FINS:

Increase heat transfer rate for a fixed surface temperature,

or

Lower surface temperature for a fixed heat transfer rate Newton's law of cooling

Examples of fins:

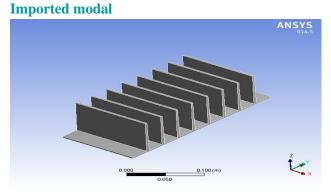
- Thin rods on the condenser in back of refrigerator.
- Honeycomb surface of a car radiator.
- Corrugated surface of a motorcycle engine.
- Coolers of PC boards.



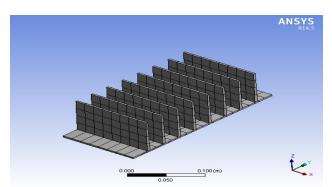
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OUTLET

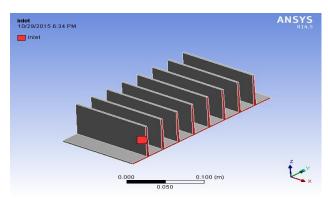
FINS ORINIGINAL MODEL



Mesh modal

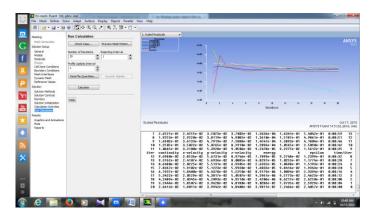


INLET



Model	Model Constants				
 Inviscid Laminar Spalart-Allmaras (1 eqn) 	Cmu ^				
 Spalai (Alima as (Teqli) k-epsilon (2 eqn) k-omega (2 eqn) Transition k-kl-omega (3 eqn) 	C1-Epsilon 1.44				
 Transition SST (4 eqn) Reynolds Stress (5 eqn) Scale-Adaptive Simulation (SAS) 	C2-Epsilon				
-epsilon Model ◎ Standard ○ RNG	TKE Prandti Number				
Realizable	User-Defined Functions Turbulent Viscosity				
Standard Wall Euroctions	none 👻				
Scalable Wall Functions	Prandtl Numbers				
Non-Equilibrium Wall Functions	TKE Prandtl Number				
User-Defined Wall Functions	none 👻				
	TDR Prandtl Number				
Options	none 👻				
Viscous Heating	Energy Prandtl Number				

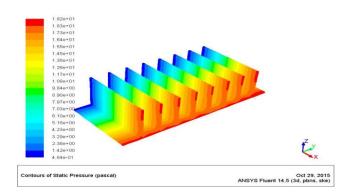
Solution Iterations Graph



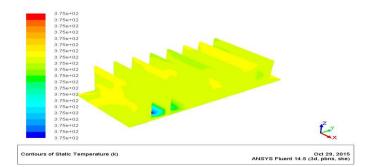


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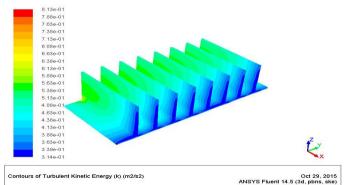
Static Pressure



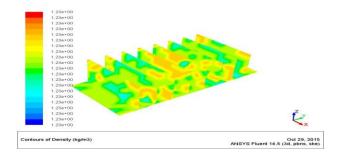
Static Temperature



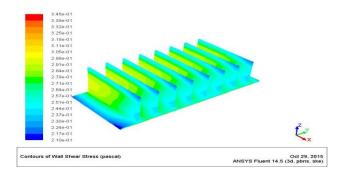
Turbulence



Density

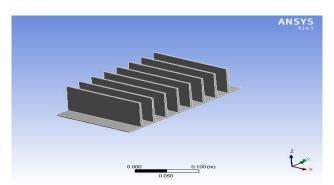


Wall fluxes

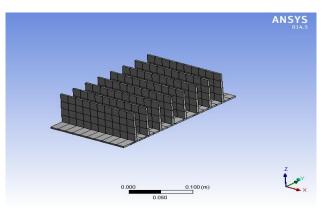


FINS LENGTH MODIFY MODEL

Import modal



Mesh modal



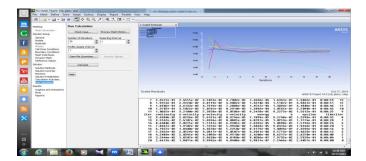
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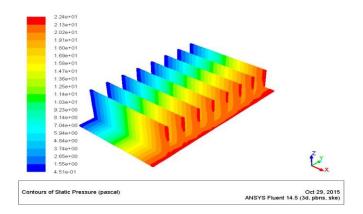
SPECIFYING BOUNDARIES FOR INLET AND OUTLET

Model	Model Constants			
Invised Laminar Spalart-Alinaras (1 eqn) K-epsilon (2 eqn) K-omega (2 eqn) K-omega (2 eqn) K-omega (3 eqn) Transition SST (4 eqn) Reynolds Stress (5 eqn) Scale-Adaptive Simulation (SAS)	Cmu ^ 0.09 C1-Epsilon E C2-Epsilon E C2-Epsilon E 1.92			
epsilon Model Standard RNG Realizable	TKE Prandtl Number			
Near-Wall Treatment Standard Wall Functions Scalable Wall Functions Non-Equilibrium Wall Functions Enhanced Wall Treatment User-Defined Wall Functions Options	Turbulent Viscosity Inone Prandtl Numbers TOR. Prandtl Number TOR. Prandtl Number			
Viscous Heating Curvature Correction	Inone Energy Prandtl Number Inone			

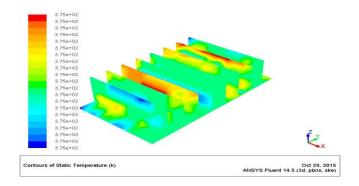
Solution Iterations Graph



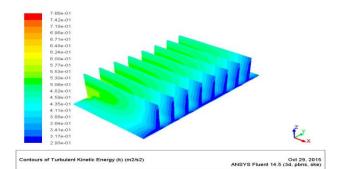
Static Pressure



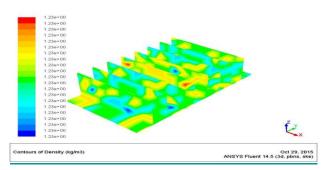
Static Temperature



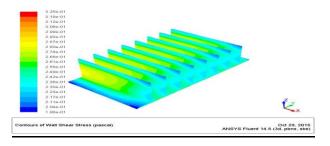
Turbulence



Density



Wall fluxes



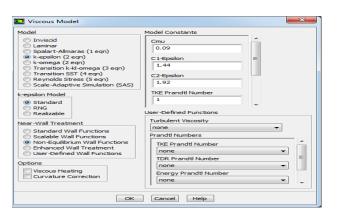
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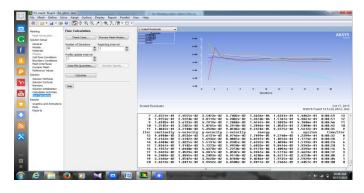
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FINS SPACE MODIFY MODEL

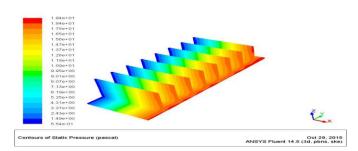
SPECIFYING BOUNDARIES FOR INLET AND OUTLET



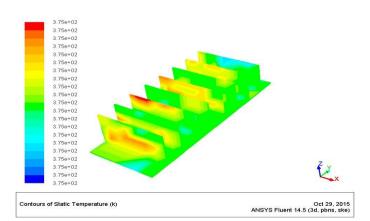
Solution Iterations Graph



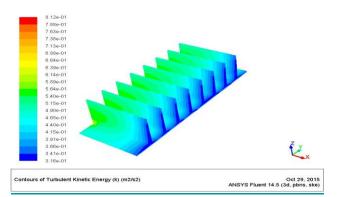
Static Pressure



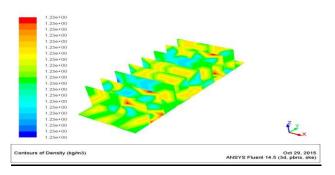
Static Temperature



Turbulence



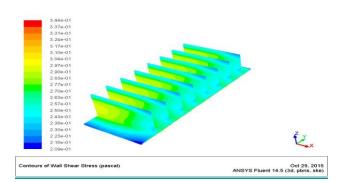
Density





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Wall fluxes

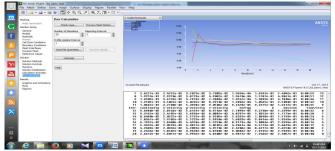


FINS THICKNESS MODIFY MODEL

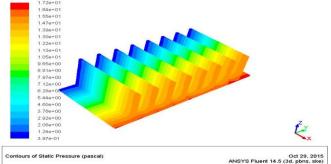
SPECIFYING BOUNDARIES FOR INLET AND OUTLET

Viscous Model	×)
Viscous Model Nodel Inviscid Laminar Spalart-Allmaras (1 eqn) K-epsilon (2 eqn) Transition S47 (4 eqn) Reynolds Stress (5 eqn) Scale-Adaptive Simulation (SAS) k-epsilon Model Standard RNG Realizable Near-Wall Treatment Standard Wall Functions Scalable Wall Functions Enhanced Wall Functions Enhanced Wall Functions Enhanced Wall Functions Dptions Viscous Heating Curvature Correction	Model Constants Cmu 0.09 C1-Epsilon 1.44 C2-Epsilon 1.92 TKE Prandtl Number 1 User-Defined Functions Turbulent Viscosity none Prandtl Numbers TKE Prandtl Number none Energy Prandtl Number Energy Prandtl Number none
OK	Cancel Help

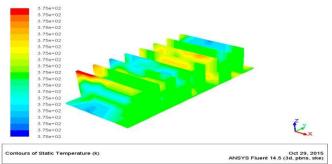
Solution Iterations Graph



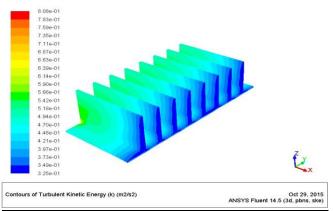
Static Pressure



Static Temperature

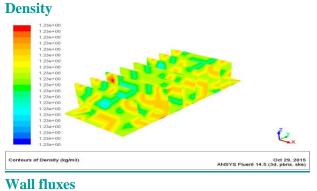


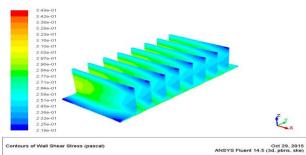
Turbulence





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RESULTS TABLE

			tem					
			per	Turbulent		De		
	Static		atur	kinetic		nsi	Wall	
	pressure		e	energy		ty	fluxes	
						Ov		
Type of	Mi	Μ	Ove	Mi	Ma	era	Mi	Μ
model	n	ax	rall	n	Х	11	n	ax
	4.	1.9				1.2	2.	3.
	84	2e	3.7	3.1	8.1	3e	10	45
Original	e-	+0	5e+	4e-	3e-	+0	e-	e-
model	01	1	02	01	01	0	01	01
	4.	2.2				1.2	1.	3.
Length	51	4e	3.7	2.9	7.6	3e	98	23
modifie	e-	+0	5e+	3e-	бе-	+0	e-	e-
d model	01	1	02	01	01	0	01	01
	5.	1.9				1.2	2.	3.
Space	54	4e	3.7	3.1	8.1	3e	09	44
modifie	e-	+0	5e+	бе-	2e-	+0	e-	e-
d model	01	1	02	01	01	0	01	01
Thickne	3.	1.7				1.2	2.	3.
SS	97	2e	3.7	3.2	8.0	3e	19	46
modifie	e-	+0	5e+	5e-	8e-	+0	e-	e-
d model	01	1	02	01	01	0	01	01

CONCLUSION

Acording to the above results we can say that heat transfer rate or total heat transfer may vary based on thermal fuexe and turbulance generated we can also get same heat transfer in a model with less surface area by creating more space for turbulant flow, more over it is also iportant that the thick ness of the fin should be adiquate

When we compare the maximim presures developed in the models the maximum presure is recrded in length modified model as they creat a more turbulence then the other models these high length fins are capable of creating hi turbulent flows

Maximum turbulent kinetic energy is recorded in space modified because here there is more scope for the wind to flow smothly and creat enough turbulance even though the pressurs are slightly low when comparred with the model two

Coming to wall fluxes which are very important to desipate the heat from the body, the highest fluxes are developed in the thickest fin ,from this it is evident that to get maximum heat transfer thickness also maters

Finally we conclude that forth model wich have less aspect ratio and more spacing between fins is the best model becacue even tough model one and model four have almost same but the material requirment for the model four is much less than model one

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AUTHOR DETAILS

1. <u>STUDENT</u>

GONAVATH DEVENDRA NAIK Received the BTech Degree in Mechanical Engineering From Dr.Samuel George Institute Of Engineering and Technology, Markapur, JNTUK, Andhra Pradesh, India, In 2013 Year, and Pursuing MTech In Thermal Engineering from Kakinada Institute of Technology & Science, Divili, Andhra Pradesh, India.

2. <u>GUIDE 1</u>

Mr. K.Mohan Krishna, Assistant professor, Kakinada institute of technology & science, Divili, Andhra Pradesh, India.

3. <u>GUIDE 2</u>

Mr. Sanmala Rajasekhar, Associate professor, Kakinada institute of technology & science, Divili, Andhra Pradesh, India.