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CFD and Thermal Analysis of FIN Tube Evaporator

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ABSTRACT:

An evaporator is used in an air-conditioning system or refrigeration system to allow a compressed cooling chemical, such as Freon or R-22, to evaporate from liquid to gas while absorbing heat in the process. It can also be used to remove water or other liquids from mixtures. The process of evaporation is widely used to concentrate foods and chemicals as well as salvage solvents. In the concentration process, the goal of evaporation is to vaporize most of the water from a solution which contains the desired product.

In this thesis, different shapes of fins in fin tube evaporator are modeled in 3D modeling software Pro/Engineer. The fins considered are continuous rectangular fin, interrupted rectangular fin, continuous circular fin, interrupted circular fin and tapered fin. The mass flow rate and heat transfer rate are analyzed by CFD analysis done in Ansys. CFD analysis is done by varying fluids R600A, R32 and R410A on all the models.

The inputs of CFD analysis are velocity and pressure and the results determined are Pressure, Velocity, Mass Flow Rate, Heat Transfer Rate and Heat Transfer Coefficient.

Thermal analysis is done by considering Aluminum alloy for fins and Copper for tubes.

INTRODUCTION

An air conditioner (often referred to as AC) is a home appliance, system, or mechanism designed to dehumidify and extract heat from an area. The cooling is done using a simple refrigeration cycle. In construction, a complete system of heating, ventilation and air conditioning is referred to as "HVAC". Its Smt. V.Saritha Ellenki College of Engineering and Technology, Patelguda(V), Hyderabad, Telangana, India.

purpose, in a building or an automobile, is to provide comfort during either hot or cold weather.



A typical home air conditioning unit

CFD ANALYSIS OF FIN TUBE EVAPORATOR BY VARYING DIFFERENT PARAMETERS RECTANGULAR FIN WITH TUBE FLUID- R32 IMPORTED MODEL



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MESHED MODEL







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EVAPORATOR CONTINUOUS RECTANGULAR FIN WITH TUBE IMPORTED MODEL



MESHED MODEL



INLET& OUTLETS





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FLUID- R32 EVAPORATOR- INTERRUPTED CIRCULAR FIN WITH TUBE IMPORTED MODEL



MESHED MODEL



INLET& OUTLETS



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THERMAL ANALYSIS OF FIN TUBE EVOPARATOR CONTINUOUS CIRCULAR FIN WITH TUBE FLUID –R32 IMPORTED MODEL



MESHED MODEL



BOUNDARY CONDITION





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TEMPERATURE



HEAT FLUX



FLUID –R600A TEMPERATURE



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HEAT FLUX FLUID –R410A TEMPERATURE



HEAT FLUX



INTERRUPTED CIRCULAR FIN WITH TUBES FLUID –R32 TEMPERATURE





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HEAT FLUX



FLUID –R600A TEMPERATURE



HEAT FLUX



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FLUID –R410A TEMPERATURE



HEAT FLUX



CONTINUOUS RECTANGULAR FIN WITH TUBE FLUID –R32 TEMPERATURE





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FLUID –R410A TEMPERATURE



INTERRUPTED RECTANGULAR FIN WITH TUBE FLUID – R32

TEMPERATURE



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HEAT FLUX



FLUID –R600A TEMPERATURE



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FLUID –R410A TEMPERATURE



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TAPERED FIN WITH TUBE FLUID –R32 TEMPERATURE



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FLUID – R600A TEMPERATURE



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FLUID –R410A TEMPERATURE



HEAT FLUX



TABLES CFD ANALYSIS RESULTS TABLE CONTINOUS CIRCULAR FIN WITH TUBE

Flui ds	Pressur e(Pa)	Velocity (m/s)	Heat transf er coeffic ient (W/m ² -k)	Mass flow rate (Kg/s)	Heat transf er rate(W)
R32	1.34E+0	3.16E+0	7.50E	1.287	0.350
	5	1	+04	4E-05	7
R60 0A	6.27E+0 4	1.43E+0 1	8.61E +04	3.182 88E- 05	1.288 1318
R41	1.21E+0	2.80E+0	5.68E	4.398	1.276
0A	5	1	+04	8E-05	24

INTRRUPTED CIRCULAR FIN WITH TUBE

Flui ds	Pressur e(Pa)	Velocit y(m/s)	Heat transf er coeffi cient (W/m ²-k)	Mass flow rate (Kg/s)	Heat transf er rate(W)
R32	1.32E+	3.16E+0	7.50E	1.5497	0.5702
	05	1	+04	2E-05	3413
R60	6.18E+	1.42E+0	8.65E	4.1246	1.6296
0A	04	1	+04	41E-05	179
R41	1.20E+	2.78E+0	5.71E	0.0001	4.4433
0A	05	1	+04	61170	562

CONTINOUS RECTANGULAR FIN WITH TUBE

Flui ds	Pressur e(Pa)	Velocity (m/s)	Heat transf er coeffi cient (W/m ²-k)	Mass flow rate (Kg/s)	Heat transf er rate(W)
R32	1.195E+	3.00E+0	7.14E	0.0011	37.73
	05	1	+04	6300	8019
R60	6.02E+0	1.38E+0	8.05E	0.0013	53.96
0A	4	1	+04	2584	7663
R41	1.17E+0	2.71E+0	5.35E	0.0012	34.06
0A	5	1	+04	6147	4296

INTRRUPTED RECTANGULAR FIN WITH TUBE

Flui ds	Pressur e(Pa)	Velocity (m/s)	Heat transf er coeffic ient (W/m ² -k)	Mass flow rate (Kg/s)	Heat transf er rate(W)
R32	1.41E+0	3.04E+0	7.58E	0.000	15.89
	5	1	+04	4985	4343
R60 0A	6.37E+0 4	1.40E+0 1	8.71E +04	7.188 32E- 05	2.613 4137
R41	1.16E+0	2.75E+0	5.75E	0.000	24.10
0A	5	1	+04	8912	5978

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TAPERED FIN WITH TUBE

Flui ds	Pressur e(Pa)	Velocit y(m/s)	Heat transf er coeffi cient (w/m ² -k)	Mass flow rate (kg/s)	Heat transf er rate(W)
R32	1.11E+	3.04E+0	7.56E	7.1525E	2.359
	05	1	+04	-05	0117
R60	5.41E+	1.40E+0	8.68E	0.00031	12.81
0A	04	1	+04	29	2933
R41	1.24E+	2.75E+0	5.73E	0.00018	5.214
0A	05	1	+04	85891	5905

CONCLUSION

In this thesis, different shapes of fins in fin tube evaporator are modeled in 3D modeling software Pro/Engineer. The fins considered are continuous rectangular fin, interrupted rectangular fin, continuous circular fin, interrupted circular fin and tapered fin.

CFD analysis is done by varying fluids R600A, R32 and R410A on all the models. By observing CFD analysis results, the pressure drop is more for interrupted rectangular fin, heat transfer coefficient is more for interrupted rectangular fin and mass flow rate and heat transfer rate are more for continuous rectangular fin. By comparing the results between refrigerants, pressure drop is more when R32 is used, heat transfer coefficient and heat transfer rate are more when R600A is used.

Thermal analysis is done by considering Aluminum alloy for fins and Copper for tubes. By observing the heat flux values, the values are more for tapered fin due to less area than rectangular and circular fins. So heat transfer rate is more for tapered fin. When R600A is used, heat flux is more.

So it can be concluded that using refrigerant R600A for rectangular continuous fin is better.

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